

ORIGINAL

BEFORE THE FLORIDA PUBLIC SERVICE COMMISSION

In Re: Joint Petition for)
Determination of Need for the Osprey)
Energy Center in Polk County by)
Seminole Electric Cooperative, Inc.)
and Calpine Construction Finance)
Company, L.P.)
_____)

DOCKET NO. 001748-EC

DIRECT TESTIMONY AND EXHIBITS

OF

TED S. BALDWIN

ON BEHALF OF

CALPINE CONSTRUCTION FINANCE
COMPANY, L.P.

DOCUMENT NUMBER-DATE

~~10477~~ DEC -4 8

FPSC-RECORDS/REPORTING

BEFORE THE FLORIDA PUBLIC SERVICE COMMISSION

IN RE: JOINT PETITION FOR DETERMINATION OF NEED FOR THE OSPREY ENERGY CENTER IN POLK COUNTY BY SEMINOLE ELECTRIC COOPERATIVE, INC. AND CALPINE CONSTRUCTION FINANCE COMPANY, L.P.

DIRECT TESTIMONY OF TED S. BALDWIN, P.E.

1 Q: Please state your name and business address.

2 A: My name is Ted S. Baldwin, and my business address is Two
3 Urban Center, 4890 West Kennedy Boulevard, Suite 600, Tampa,
4 Florida, 33609.

5
6 Q: Where are you employed and in what position?

7 A: I am employed by Calpine Eastern Corporation as a Regional
8 Engineer.

9
10 Q: Please describe your duties with Calpine Corporation.

11 A: I am responsible for the technical aspects related to the
12 development of power plant projects. These responsibilities
13 include selection of the plant configuration, the preliminary
14 plant layout, calculation of plant performance, and oversight
15 of the environmental permitting process.

16

17

QUALIFICATIONS AND EXPERIENCE

18 Q: Please summarize your educational background and experience.

19 A: I received a Bachelor of Science degree in Mechanical
20 Engineering from the University of Texas in Austin in 1981.

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1 I also received a Masters of Science degree in Mechanical
2 Engineering from the University of Michigan in 1982.

3

4 **Q: Please summarize your experience in power plant design,**
5 **engineering, construction, operations, permitting, and**
6 **licensing.**

7 A: I have approximately 18 years of experience in the electric
8 power industry, working as an equipment engineer, analytical
9 engineer, boiler engineer, thermal cycle systems engineer,
10 engineering group manager, director of engineering and now
11 Regional Engineer for Calpine Eastern Corporation. In those
12 positions, I have gained a wide range of experience in
13 electrical power plant design, engineering, construction,
14 operations, permitting and licensing. As part of my job, I
15 have assisted in the design of more than a dozen gas-fired
16 electrical generating plants. Exhibit _____ (TSB-1) is my
17 current resume'.

18

19 **Q: Are you a member of any professional organizations?**

20 A: I have been a member of the American Society of Mechanical
21 Engineers for the past twelve years.

22

23

24

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SUMMARY AND PURPOSE OF TESTIMONY

1

2 Q: What is the purpose of your testimony?

3 A: I am testifying on behalf of Calpine Construction Finance
4 Company, L.P. ("Calpine"), one of the joint applicants for the
5 Commission's determination of need for the Osprey Energy
6 Center (the "Osprey Project" or "Project"). I will describe
7 the main design features of the Project, as well as the
8 Project's operational reliability and flexibility. I also
9 will describe the performance characteristics and
10 environmental profile of the Project, and present the
11 engineering, procurement, and construction schedule for the
12 Project.

13

14 Q: What are your responsibilities with respect to the Osprey
15 Project?

16 A: In my position as Regional Engineer for Calpine Eastern
17 Corporation, I oversee the preliminary engineering effort and
18 regulatory support activities associated with the Project.

19

20 Q: Please summarize the key features of the Project.

21 A: The Osprey Project is a state-of-the-art natural gas-fired
22 combined cycle generation facility. The plant will have
23 approximately 529 megawatts ("MW") of net generating capacity
24 based on anticipated manufacturer's guarantees at average

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1 ambient site conditions. The Osprey Project's rated winter
2 capacity will be approximately 578 MW and its rated summer
3 capacity will be approximately 496 MW. The Osprey Project
4 will have a high thermal efficiency with a projected heat rate
5 of approximately 6800 British thermal units ("Btu") per
6 kilowatt-hour ("kWh"), based on the Higher Heating Value
7 ("HHV") of natural gas at ambient site conditions. The
8 Project will utilize state-of-the-art dry low-NO_x combustion
9 technology to minimize emissions of nitrogen oxides (NO_x). In
10 addition, a selective catalytic reduction ("SCR") system will
11 be used to further reduce NO_x emissions.

12 The Osprey Project will be a highly reliable power
13 generation facility, with an estimated annual equivalent
14 availability factor of approximately 94.5 percent. The
15 operations and maintenance plan for the Project will be in
16 accordance with the equipment manufacturer's recommended
17 maintenance schedules.

18

19 **Q: Are you sponsoring any exhibits to your testimony?**

20 **A: Yes. I am sponsoring the following exhibits.**

21 (TSB-1): Current resume' of Ted S. Baldwin.

22 (TSB-2): Osprey Energy Center, Project Profile.

23 (TSB-3): Osprey Energy Center, Site Plan.

24 (TSB-4): Osprey Energy Center, Proposed Plot Plan.

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1 (TSB-5): Osprey Energy Center, Computer-Generated
2 Perspective Rendition.

3 (TSB-6): Estimated Plant Performance and Emissions.

4 (TSB-7): Osprey Energy Center, Cycle Schematic Diagram.

5 (TSB-8): Summary of the Design Basis for the Project.

6 (TSB-9): Osprey Energy Center, Electrical One-Line Diagram.

7 (TSB-10): Preliminary Average Annual Water Balance for the
8 Project.

9 (TSB-11): Preliminary Peak Month Daily Water Balance for the
10 Project.

11 (TSB-12): EPC Schedule for the Project.

12 I am also sponsoring Tables II-2 and II-3 and Figures II-
13 3 through II-10 and II-15 in Volume II of the Exhibits to the
14 Joint Petition for Determination of Need filed with the
15 Commission concurrently with this testimony, and the text that
16 accompanies those tables and figures.

17

18 **PROJECT DESCRIPTION AND ENGINEERING DESIGN**

19 **Q: Please describe the Osprey Project.**

20 **A:** The Osprey Project is a state-of-the-art natural gas-fired
21 combined cycle generation facility. The plant consists of two
22 combustion turbine generators ("CTGs"), two heat recovery
23 steam generators ("HRSGs") and one steam turbine generator
24 ("STG"). The Project will use wet cooling towers to condense

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1 steam back to water for reuse in the HRSGs and STG. The plant
2 will have approximately 529 MW of net generating capacity
3 (based on anticipated manufacturer's guarantee) at average
4 ambient site conditions. The average ambient conditions at
5 the Project site are 74°F. and 80% relative humidity. A
6 general profile of the Project is shown in Exhibit ____ (TSB-
7 2).

8 The Project will also have a net output capability,
9 without duct-firing or power augmentation, of 545 MW (nominal)
10 at ISO temperature (59°F.) and relative humidity (60%)
11 conditions.

12 The Project will utilize dry low-NO_x combustion
13 technology to minimize emissions of NO_x. In addition, an SCR
14 system will be used to further reduce NO_x emissions.

15

16 **Q: Please describe the SCR system that will be used to reduce the**
17 **Project's NO_x emissions.**

18 **A:** The SCR system for the Project will consist of a catalyst and
19 an ammonia injection grid located within the HRSG. When NO_x
20 is exposed to ammonia in the presence of the catalyst, the NO_x
21 is converted to elemental nitrogen and oxygen.

22

23 **Q: Please give a brief description of the site for the Osprey**
24 **Project.**

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1 A: The site for the Project consists of approximately 19.5 acres,
2 situated approximately 1.5 miles southwest of downtown
3 Auburndale, in Polk County. The site is a non-producing
4 citrus grove and is currently unused. A detailed description
5 of the Project site is presented in the testimony of Mr.
6 Richard Zwolak, AICP, in support of the Project, and in the
7 exhibits that he is sponsoring in support of the Project.

8

9 **Q: Please summarize the general arrangement and layout of the**
10 **Project on the site.**

11 A: The general arrangement of the Project is shown on the Site
12 Plan in Exhibit ____ (TSB-3). Exhibit ____ (TSB-4) shows a
13 detailed layout of the main Project structures on the site,
14 and Exhibit ____ (TSB-5) presents a computer-generated
15 perspective rendition of the Project.

16

17 **Q: Please describe the generating technology of the Osprey**
18 **Project.**

19 A: The Osprey Energy Center will have an expected net output
20 capability, without duct-firing or power augmentation, of
21 approximately 529 MW based on the anticipated manufacturer's
22 guarantee at average ambient site conditions. As I previously
23 noted, the power block will consist of two advanced technology
24 Siemens-Westinghouse Model 501F CTGs, two matched HRSGs that

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1 include duct-firing capability, and one STG, which has the
2 ability to utilize steam for power augmentation to increase
3 output from the CTGs.

4

5 **Q: Please define the terms "duct-firing" and "power**
6 **augmentation."**

7 A: Duct-firing is a process whereby additional gas burners are
8 placed within the HRSGs to increase the gas temperature and
9 generate more steam, thus increasing power generation from the
10 STG. Power augmentation refers to a process in which steam
11 from the HRSGs is injected into the gas turbines for the
12 purpose of increasing mass flow through the CTGs, thereby
13 increasing the electrical power output from the CTGs.

14

15 **Q: What will the peak generating capacity of the Osprey Project**
16 **be?**

17 A: Without duct-firing and power augmentation, the Osprey
18 Project's rated winter capacity will be approximately 578 MW
19 and its rated summer capacity will be approximately 496 MW.
20 With duct-firing and power augmentation, the Project's winter
21 capacity will be approximately 666 MW and its summer capacity
22 will be approximately 575 MW.

23

24 **Q: What are the Osprey Project's expected heat rate and thermal**

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1 **efficiency?**

2 **A:** The Project is projected to have a heat rate of approximately
3 6,800 Btu per kWh, based on the HHV of natural gas at average
4 ambient site conditions, reflecting a net thermal efficiency
5 of approximately 50.2 percent.

6

7 **Q: Please describe the performance characteristics of the Osprey**
8 **Project.**

9 **A:** The performance characteristics of the generating facility are
10 summarized in the Plant Performance Table, Exhibit _____
11 (TSB-6). This table presents facility generating output and
12 emissions data for the Project at various expected ambient
13 site conditions, at full and part load operation.

14

15 **Q: Please describe the power generation cycle for the Project.**

16 **A:** The power generation cycle of the Project is depicted on the
17 overall cycle schematic diagram for the Project on Exhibit
18 ____ (TSB-7). In brief, natural gas is burned in the CTG
19 where the expanding combustion gases turn the CTG's shaft to
20 produce electricity; and exhaust gases exit the CTG and enter
21 the HRSG at approximately 1100°F. Two HRSGs, one per CTG, are
22 used to recover heat from the exhaust gases by producing steam
23 at three different pressure levels. The steam produced in the
24 HRSGs is then expanded through a single STG to produce

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1 additional electrical power. The successive uses of thermal
2 energy, first in the CTGs and second in the HRSGs and STG, to
3 produce electricity is why this generating technology is
4 called "combined cycle."

5

6 **Q: Please describe the design basis for the Project.**

7 A: The design basis for the Project is summarized in Exhibit ____
8 (TSB-8). The description contained in Exhibit _____ (TSB-8)
9 is accurate and is hereby incorporated by reference into my
10 testimony.

11

12 **Q: Please describe the basic electrical characteristics of the**
13 **Osprey Project.**

14 A: The basic electrical characteristics of the Project are set
15 forth in the Project's electrical one-line diagram, Exhibit
16 _____, (TSB-9). In brief, electrical power is produced at 18
17 kilovolts (kV) in the CTGs and 16 kV in the STG. Each
18 generator is connected to a transformer which steps up the
19 electrical voltage to 230 kV, which is the operating voltage
20 of the Tampa Electric Company ("TECO") transmission system in
21 the vicinity of the Osprey Project. Electricity is delivered
22 to the transmission system through the Recker high voltage
23 substation owned by TECO. This substation is an existing
24 substation that will be expanded to accommodate the

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1 interconnection of the Project.

2

3 **Q: Please describe the projected fuel use for the Project.**

4 A: At full load, the Project will use approximately 86 million
5 standard cubic feet of natural gas per day at annual average
6 site conditions.

7

8 **Q: Please summarize the start-up and emergency power supplies for**
9 **the Project.**

10 A: The Project will obtain station service and start-up power
11 from Tampa Electric Company in order to maintain normal plant
12 auxiliary loads during periods in which the facility is off-
13 line and to accelerate the CTGs to a self-sustaining operating
14 speed during start-up. In the event of a loss of the
15 transmission system, emergency power for critical components
16 necessary for safe shutdown of the plant will be provided from
17 a stationary battery system. The plant is also equipped with
18 emergency diesel generators to keep the battery system charged
19 and to provide supplemental power to the plant for other loads
20 that are not critical. The plant's battery system and
21 emergency diesel generators will be capable of providing
22 sufficient power for safe shutdown of each unit and to keep
23 certain prioritized auxiliaries operating, but will not be
24 capable of restarting the units.

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1 Q: Please give a brief description of the control systems for the
2 Osprey Project.

3 A: The Project is controlled by a distributed control system
4 ("DCS"). A DCS is a fiber optic cable network that runs
5 throughout the plant that picks up control input signals such
6 as pressure, temperature, or flow, delivers the signals to the
7 central control computer and then distributes control output
8 signals such as the opening or closing of a valve or the
9 starting and stopping of a motor. The control system is
10 designed to provide full automation of the unit. The gas
11 turbine sequencer allows the operator to start and stop the
12 gas turbines automatically. Operator stations are designed to
13 allow a graphical, intuitive navigation through the plant
14 processes from a central control room.

15

16 OPERATIONAL RELIABILITY

17 Q: Please discuss the operational reliability of the Osprey
18 Project.

19 A: The Osprey Project will have a high degree of reliability
20 similar to other state-of-the-art combined cycle generating
21 facilities.

22 Reliability is often measured in terms of the percentage
23 of hours a unit is available to produce electricity within a
24 specified period of time, usually one year. The Osprey

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1 Project is expected to achieve an annual equivalent
2 availability factor of 94.5 percent. This factor will vary
3 depending on the planned maintenance activities in a given
4 year, the forced outage rate, the need to take the CTGs off-
5 line to clean compressor blades, and the need to perform
6 occasional minor maintenance.

7

8 **Q: What are the expected forced outage and maintenance outage**
9 **rates for the Osprey Project?**

10 **A:** The forced outage rate for the plant is expected to average
11 approximately two percent per year.

12 The maintenance (also known as planned) outage rate for
13 the plant is expected to average 3.5 percent per year, but the
14 actual rate will vary from year to year in accordance with the
15 vendor's recommended maintenance cycle for the CTGs. The
16 Siemens-Westinghouse Model 501F turbines have an 8,000 hour
17 maintenance cycle. A minor inspection, referred to as a
18 combustor inspection, will be conducted at the end of each
19 8,000 hours of operation. A slightly more detailed
20 inspection, referred to as a hot gas inspection, along with
21 the combustor inspection, will be conducted at the end of
22 24,000 hours of operation. A major inspection will be
23 conducted at 48,000 hours of operation. This cycle will be
24 repeated for the life of the equipment. Combustor and hot gas

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1 inspections take approximately 7 days and 14 days
2 respectively, and a major inspection takes approximately 21
3 days.

4
5 **Q: Who will operate the Osprey Project?**

6 **A:** The Osprey Project will be operated either by an operating
7 subsidiary of Calpine or by a subcontractor engaged for that
8 purpose by Calpine.

9
10 **Q: Please describe any special design features or other**
11 **considerations that are relevant to the Osprey Project's**
12 **operational reliability.**

13 **A:** The Osprey Project will be constructed utilizing the most
14 advanced CTG design with extensive operating experience. The
15 building configuration and balance of plant equipment will be
16 typical of designs used throughout the industry for combined
17 cycle plants. Use of such standard equipment offers the
18 highest possible reliability.

19

20

ENVIRONMENTAL PROFILE

21 **Q: Please summarize the environmental profile of the Osprey**
22 **Project.**

23 **A:** The Project will be fueled by natural gas. The Project has
24 been designed with careful consideration of environmental

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1 issues and will be one of the cleanest power plants in Florida
2 and in the United States. It will utilize dry low-NO_x
3 combustion technology and an SCR system to minimize NO_x
4 emissions. The Project's emissions of critical pollutants are
5 projected to be approximately as follows (based on an average
6 ambient conditions of 74°F., 80% relative humidity, with both
7 CTGs operating at 100% load, and without power augmentation or
8 duct-firing):

9 Sulfur Dioxide: negligible, less than 19.8 lbs. per hour
10 (less than 87 tons per year)

11 Nitrogen Oxides: 3.5 parts per million dry volume at 15%
12 oxygen, or 46.3 lbs. per hour (203 tons
13 per year)

14 Volatile Organic Compounds: 10.4 lbs. per hour (46 tons
15 per year)

16 Particulate Matter: 40.1 lbs. per hour (176 tons per year) as
17 PM₁₀

18 Carbon Monoxide: 10 parts per million dry volume at 15%
19 oxygen, 82 lbs. per hour (359 tons per
20 year)

21 Operation of the Project is likely to result in
22 measurable reductions in emissions of SO₂, CO₂, NO_x, and other
23 air pollutants in Peninsular Florida, due to the Project's
24 displacement of generation from: (a) units that burn fuels

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1 that produce more pollution than is produced by the natural
2 gas fuel used in the Project, (b) less efficient units, and
3 (c) units that do not include the types of pollution controls
4 being utilized by the Project.

5
6 **Q: Please summarize the projected water requirements and water**
7 **supply plan for the Osprey Energy Center Project.**

8 **A:** The Project will require approximately 3.55 million gallons
9 per day ("MGD") of water calculated on an annual average
10 basis. At peak conditions with power augmentation and duct-
11 firing for six hours per day, the Project will require
12 approximately 4.79 MGD of water.

13 The Osprey Project will utilize a combination of
14 reclaimed water and ground water for its process and makeup
15 water supply. Reclaimed water will be supplied from the City
16 of Auburndale's Allred Wastewater Treatment Plant. The
17 Project will require the construction of reclaimed water
18 pipelines to connect with the City of Auburndale's wastewater
19 treatment facility. The pipelines to the Allred wastewater
20 treatment facilities will be approximately one mile in length
21 and will be constructed in existing public rights-of-way.
22 Additionally, other minor pipeline modifications will be made
23 to enhance discharge capability. The reclaimed water supply
24 and return pipelines to Allred will run along the north Recker

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1 Highway right-of-way to the Osprey Project site boundary. The
2 City of Auburndale will obtain the necessary permits for the
3 water and wastewater pipelines. The remainder of the Osprey
4 Project's water supply will be provided by new on-site wells
5 withdrawing water from the Upper Floridan aquifer.

6 The preliminary water balance for the Project at average
7 conditions is shown in Exhibit _____ (TSB-10), and the
8 preliminary water balance for peak monthly conditions is shown
9 in Exhibit _____ (TSB-11).

10
11 **PROJECT SCHEDULE**

12 **Q: Who will be the engineering, procurement, and construction**
13 **contractor for the Project?**

14 **A:** Calpine Corporation's construction management group will
15 manage the engineering and construction of the Osprey Project.
16 Calpine Corporation's construction management group will
17 specify and procure the major equipment for the Osprey Project
18 including the CTGs, HRSGs, and the STG. Parsons Energy and
19 Chemical Group will perform the detailed engineering for the
20 Project. Calpine Corporation's construction management group
21 will competitively bid the construction of the Osprey Project
22 to qualified general contractors with experience in the power
23 industry, such as H.B. Zachary or The Industrial Company.

24

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1 Q: Please describe the engineering, procurement, and construction
2 schedule for the Project.

3 A: The engineering, procurement, and construction schedule (the
4 "EPC schedule"), Exhibit ____ (TSB-12), provides for the
5 Project to be designed and brought into commercial service --
6 i.e., "on-line" -- by the second quarter of 2003. Preliminary
7 engineering design has already begun and detailed engineering
8 will begin in February 2001. The general contractor for
9 construction will be selected in the first quarter of 2001.
10 The Project schedule provides for approximately 24 months from
11 Project release to commercial operation.

12

13 Q: What is the current status of the engineering design work for
14 the Osprey Project?

15 A: Conceptual engineering is complete. A site plan, plot plan,
16 process flow diagram, electrical one-line diagram, water
17 balance, capital cost estimate, and operation and maintenance
18 estimate are also complete.

19

20 Q: Does this conclude your direct testimony?

21 A: Yes, it does.

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Energy Center in Polk County by)
Seminole Electric Cooperative, Inc.)
and Calpine Construction Finance)
Company, L.P.)
_____)

DOCKET NO. _____

EXHIBITS

OF

TED S. BALDWIN

ON BEHALF OF

**CALPINE CONSTRUCTION FINANCE
COMPANY, L.P.**

TED S. BALDWIN
Calpine Corporation
Two Urban Center
4890 W. Kennedy Blvd., Suite 600
Tampa, FL 33609

JOB EXPERIENCE:

REGIONAL ENGINEER, Calpine Corporation, Tampa, FL, May 2000 to present.

- Responsible for technical support of all business development activities in the Southeastern United States. Project locations include Florida, Alabama, Mississippi, and Kentucky.

Tasks managed include due diligence on existing facilities, conceptualization of project technical configuration, preparation of project heat balances, site selection and site development (including environmental permits), preparation of capital cost estimates, participation in the negotiation of power purchase agreements and tolling agreements, development and negotiation of engineering and construction contracts, review of fuel supply contracts and other project documents, and interface with financing parties regarding technical aspects of the projects.

DIRECTOR OF ENGINEERING AND CONSTRUCTION, Nations Energy Corporation (Independent Power Subsidiary of Tucson Electric Power), Winter Park, Fl., May 1995 to present.

- Involved in the startup of a new energy development company. Responsibilities include managing all technical aspects of developing domestic and international energy projects, including acquisitions and greenfield/brownfield projects. Successfully closed two projects and carried two other projects through advanced stages of development with closings expected in 1999 and 2000.

Tasks managed include due diligence on existing facilities, conceptualization of project technical configuration, site selection and site development (including environmental permits), preparation of capital cost estimates, preparation of operation and maintenance (O&M) estimates, participation in the negotiation of power purchase agreements and tolling agreements, development and negotiation of engineer, procurement, and construction (EPC) contracts and O&M agreements, review of fuel supply contracts and other project documents, and interface with financing parties regarding technical aspects of the projects. Also manage the implementation of one international EPC contract by providing direction to project manager directly responsible for the project.

Country involvement includes U.S.A. (Colorado, Florida, and Louisiana), Mexico, Panama, Honduras, Netherlands Antilles, and Czech Republic. Fuel technologies include gas, pulverized coal, waste coal, biomass, diesel, residual oil, and refinery byproducts such as refinery gas and asphalt. Projects often involve the integration of existing facilities with new facilities and the supply of power, steam, and other utilities to industrial complexes such as refineries and breweries.

Resume of
TED S. BALDWIN
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APPLICATION ENGINEERING MANAGER, Power Generation Business Unit, Westinghouse Electric Corp., Orlando, Fl., April 1992-April 1995.

- Managed a multi-disciplined group of twenty-three engineers and technicians including thermal design, mechanical design, controls, and electrical engineers. The group was responsible for the technical content of bids and the technical negotiation of all new construction orders within the business unit, including combustion turbine and steam turbine equipment, extended scope thermal island (combined cycle and conventional steam), and extended scope turnkey (simple cycle and combined cycle) projects. Annual sales in 1994 significantly in excess of one billion dollars. Responsible for technical negotiation of EPC contracts and risk management of all technical related warranties including plant performance, emissions, availability, reliability, etc. Oversaw transformation of organization into regional business teams with application engineering personnel stationed at four different locations throughout the world.

THERMAL CYCLE SYSTEM GROUP MANAGER, Power Generation Projects Division, Westinghouse Electric Corp., Orlando, Fl., April 1990-March 1992.

- Responsible for the implementation of combined cycle power projects from contract signing to completion of plant performance testing. Managed a group of ten engineers and technicians responsible for thermal cycle design, preparation of plant mass and material balances, and specification/evaluation of major thermal equipment (heat recovery steam generator, steam turbine, condenser, deaerator, cooling tower, auxiliary boiler, etc.) within the power plant. The group was also responsible for performance testing of the power plant after commissioning.

THERMAL CYCLE SYSTEMS ENGINEER, Power Generation Projects Division, Westinghouse Electric Corp., Orlando, Fl., May 1987-March 1990.

- Responsible for application support and implementation support of combined cycle power projects, mostly in the domestic market. Prepared preliminary and final cycle design, final plant mass and material balances, major equipment specifications for heat recovery steam generators, condensers, deaerators, etc. Participated in the evaluation and vendor negotiations for these pieces of equipment.

BOILER ENGINEER, Machinery Technology Division, Westinghouse Electric Corp., Pittsburgh, Pa., December 1985-April 1987.

- Provided thermal design engineering support to the U.S. Navy in the field of marine propulsion boilers.

Resume of
TED S. BALDWIN
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EQUIPMENT ENGINEER/ANALYTICAL ENGINEER, Machinery Division/Furnace Division, The M.W. Kellogg Company, Houston, Texas, June 1982-November 1985.

- Responsible for preparation of equipment specifications, evaluation of vendors' bids, requisition preparation, technical follow-up, drawing review, and performance testing on major power generation equipment items including package boilers, gas turbine waste heat recovery units, and associated auxiliaries.

EDUCATION:

Masters of Science in Mechanical Engineering, 1982. The University of Michigan, Ann Arbor. Graduate Fellowship Program. Curriculum emphasis in the thermal sciences.

Bachelor of Science in Mechanical Engineering, 1981. The University of Texas, Austin. Scholarship Program.

TABLE 2

**OSPREY ENERGY CENTER
PROJECT PROFILE**

Expected Plant Capacity:

a.	Average ambient rating (74°F, 80% R.H.):	529 MW
b.	Summer (95°F, 80% R.H.):	496 MW
	With Duct-firing & Power Augmentation:	575 MW
c.	Winter (32°F, 60% R.H.):	578 MW
	With Duct-firing & Power Augmentation:	666 MW
d.	ISO (59°F, 60% R.H.):	545 MW

Project Energy Production: Approximately 4,300,000 MWH/year
(not including duct-firing or power augmentation)

Technology Type: Two Siemens-Westinghouse 501F advanced firing temperature technology combustion turbines, two heat recovery steam generators, and one steam turbine generator in combined cycle configuration

Anticipated Construction Schedule:

a.	Engineering release date:	February 2001
b.	Construction mobilization date:	June 2001
c.	Commercial in-service date:	2nd quarter 2003

Fuel Use: Approximately 86 million Standard Cubic Feet of natural gas/day, annual average conditions (74°F, 80% R.H.), full load

Air Pollution Control Strategy: Dry low-NOx burners and SCR

Cooling Method: Wet Cooling Tower

Total Site Area: 19.5 acres (approximate)

Construction Status: Planned

Certification Status: Need Determination Petition and Site Certification Application filed.

Status with Federal Agencies: FERC has issued its order granting Calpine market-based rate authority.

TABLE 2

OSPREY ENERGY CENTER
PROJECT PROFILE
(CONTINUED)

Projected Unit Performance Data:

Planned Outage Factor (POF):	3.5%
Forced Outage Factor (FOF):	2.0%
Equivalent Availability Factor (EAF):	94.5%
Estimated Annual Average Capacity Factor (%):	91.0%

Average Net Operating Heat Rate (ANOHR): 6800 Btu/kWh (HHV)
(74°F, 80°R.H.) expected

Project Unit Financial Data (per Calpine Corporation):

Book Life (years):	35 years
Direct Construction Cost:	Approx. \$194.8 million
AFUDC Amount:	Not applicable
Escalation (\$/kW):	Not applicable
Fixed O&M (\$/kW per year):	Proprietary
Variable O&M (¢/MWH):	Proprietary
K-Factor:	Not applicable
Project Life:	35 years

Expected Plant Air Emissions: NO_x: 3.5 ppmvd @15% O₂
SO₂: 20.8 lbs/hour
CO: 10 ppm

New Transmission Lines Required: None

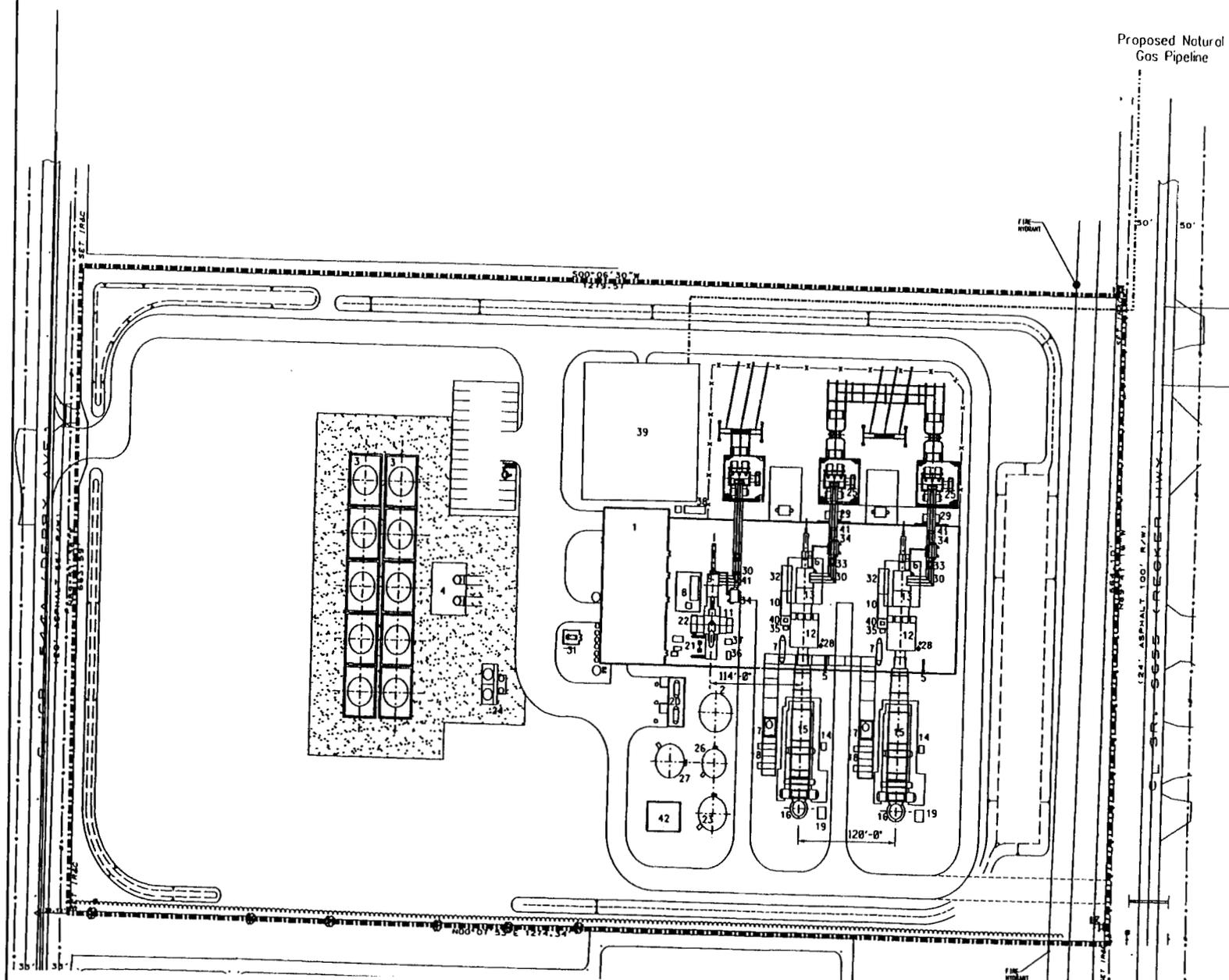
Gas Pipeline Required: None

Water Requirements: Approx. 4.79 MGD, summer peak
(Including Reclaimed Water) Conditions (95°F, 80 R.H.),
(with power augmentation and duct-firing)
Approx. 3.55 MGD average
(74°F, 80 R.H.), (without power augmentation or duct-firing)

Wastewater Discharge: Approx. 1.26 MGD. summer peak conditions (with power augmentation and duct-firing)
Approx. 0.62 MGD, average conditions (3.9 cycles of concentration without power augmentation and duct-firing)

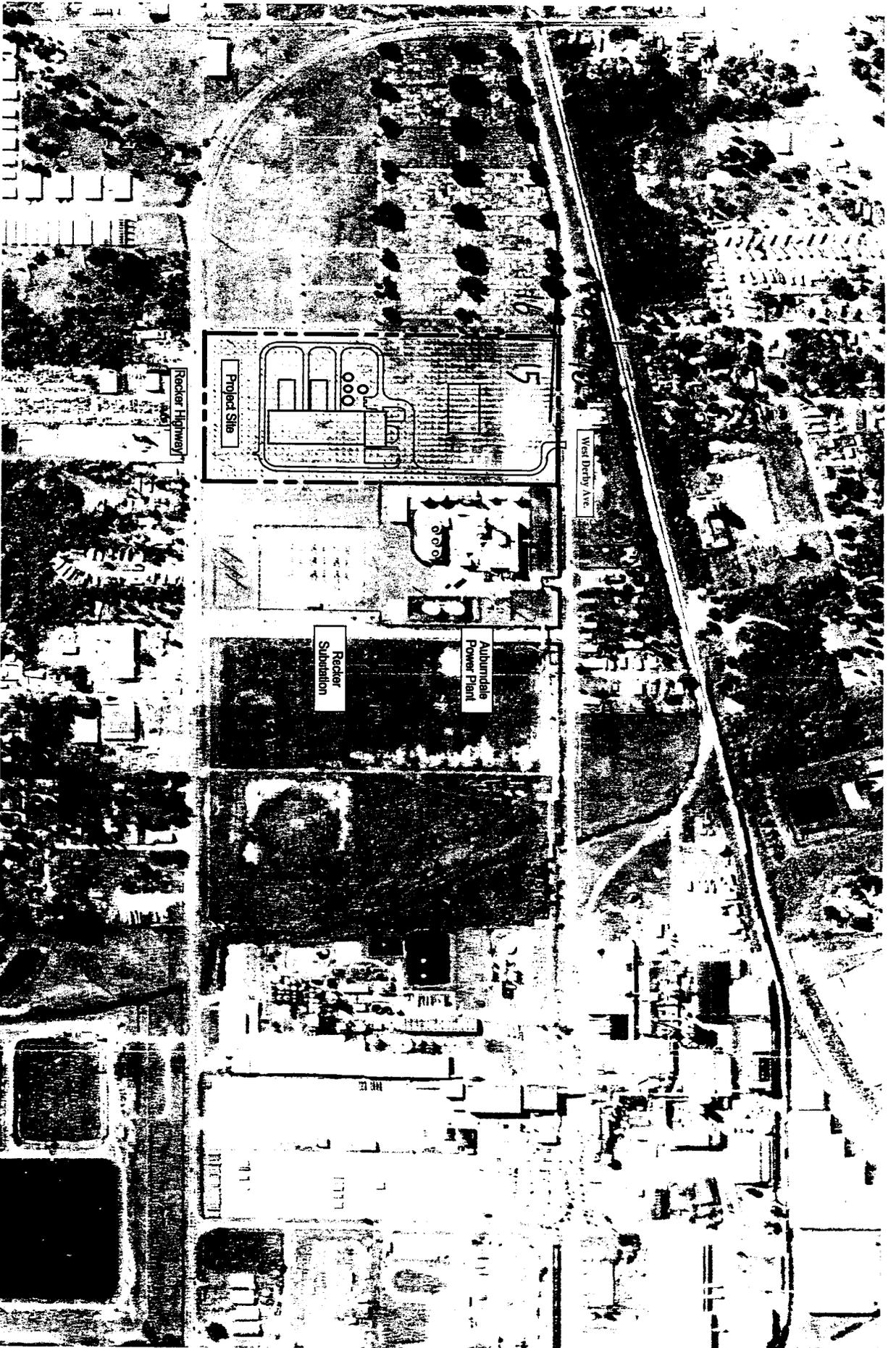
Legend

1. ADMINISTRATION AND MAINTENANCE BUILDING
2. SERVICE WATER TANK
3. COOLING TOWER
4. CIRCULATING WATER PUMPS
5. FUEL GAS HEATER
6. COMBUSTION TURBINE AIR INLET FILTER
7. KETTLE BOILER
8. LUBE OIL SKID
9. ST GENERATOR
10. CT MECHANICAL PACKAGE
11. STEAM TURBINE
12. COMBUSTION TURBINE
13. CT GENERATOR
14. AMMONIA INJECTION SKID
15. HEAT RECOVERY STEAM GENERATOR
16. HRSG STACK
17. HRSG BLOWDOWN TANK
18. BOILER FEED PUMP HOUSE
19. CEMS
20. AMMONIA STORAGE TANKS
21. CONDENSATE PUMPS
22. CONDENSER
23. DEMINERALIZED WATER STORAGE TANK
24. WET SURFACE AIR COOLER
25. GENERATOR STEP-UP TRANSFORMER
26. WASTEWATER TANK
27. RAW WATER STORAGE TANK
28. FUEL GAS SCRUBBER
29. UNIT AUX. TRANSFORMER
30. ISO-PHASE BUS DUCT
31. STANDBY GENERATOR
32. ELECTRICAL EQUIPMENT PACKAGE
33. GENERATOR VT & SURGE CUBICLE
34. GENERATOR EXCITATION SKID
35. COMPRESSOR WATER WASH SKID
36. STEAM JET AIR EJECTORS
37. GLAND STEAM CONDENSER
38. OIL/WATER SEPARATOR
39. GAS METER BUILDING
40. HYDRAULIC SKID
41. EXCITATION TRANSFORMER
42. CENTRAL PUMP HOUSE



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 Page 1 of 1

 Golder Associates Tampa, Florida	Site Plan	
	Client / Project	Job No.
	Calpine Construction Finance Company, L.P. Osprey Energy Center	993-9570
CAD BY: CDT	SCALE: 1"=120'	FIGURE Revision 1
CHK BY: HGB	DATE: 08/11/00	3.2.0-2
REV BY: -	FILE No.: fig3_2_0-2.dwg	



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 Tampa, Florida

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 Page 1 of 1

PLOT PLAN

CDR BY:	011	SCALE:	1"=400'	JOB NO.:	983-9570
CHK BY:	RAZ	DATE:	03/02/00	TRACER:	
REV BY:	-	FILE NO.:	pot-plan.dwg		

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PERSPECTIVE RENDITION

CAD BY: CDT	SCALE: NTS	Job No. 993-9570
CHK BY: RAZ	DATE: 03/04/00	FIGURE
REV BY: -	FILE No.: fig1_3_3-1.dwg	

Tampa, Florida

Calpine Construction Finance Company, L.P.
 Osprey Energy Center



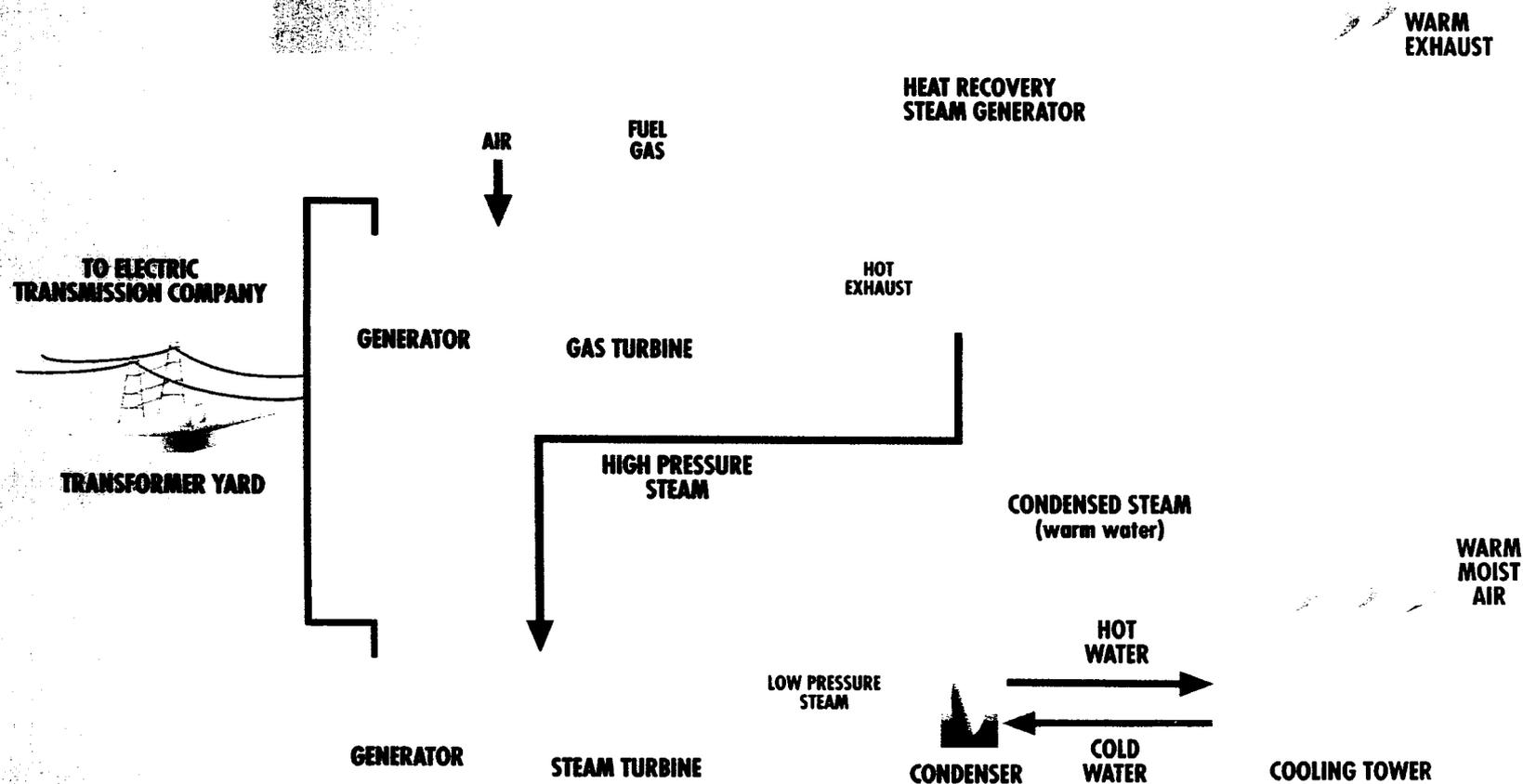
Client / Project

TABLE 2
OSPREY ENERGY CENTER
Estimated Plant Performance and Emissions Data

		100%	100%	100%	100%	70%	70%	70%	70%	60%	60%	60%	60%	100%
Percent Load		100%	100%	100%	100%	70%	70%	70%	70%	60%	60%	60%	60%	100%
Ambient Temperature	F	95	74	59	32	95	74	59	32	95	74	59	32	95
Ambient Relative Humidity	%	80%	80%	60%	60%	80%	80%	60%	60%	80%	80%	60%	60%	80%
Gas Turbine Power	MW	324	347	362	390	222	240	253	272	190	205	216	233	357
Steam Turbine Power	MW	185	195	197	203	145	153	152	154	135	143	149	148	233
Net Cycle Power	MW	496	529	545	578	358	383	395	416	317	339	356	371	575
Net Cycle LHV Heat Rate	BTU/kW-hr	6,187	6,122	6,125	6,137	6,497	6,430	6,359	6,373	6,599	6,529	6,478	6,457	6,576
Net Cycle LHV Efficiency	%	55.2%	55.7%	55.7%	55.6%	52.5%	53.1%	53.7%	53.5%	51.7%	52.3%	52.7%	52.9%	51.9%
Net Cycle HHV Heat Rate	BTU/kW-hr	6,871	6,798	6,802	6,815	7,215	7,140	7,062	7,077	7,329	7,251	7,193	7,170	7,303
CTG fuel flow (lb/h)- total for two CTGs	lb/hr	146,325	154,237	159,099	168,918	110,864	117,346	119,634	126,212	99,806	105,621	109,911	114,296	155,858
CTG heat input, HHV basis (mmBtu/h)- total for two CTGs	MMBtu/hr	3,409	3,594	3,707	3,936	2,583	2,734	2,787	2,941	2,325	2,461	2,561	2,663	3,631
Duct burner fuel flow (lb/h)- total for two burners	lb/hr	0	0	0	0	0	0	0	0	0	0	0	0	24,308
Duct burner heat input, HHV basis (mmBtu/h)- two burners	MMBtu/hr	0	0	0	0	0	0	0	0	0	0	0	0	566
CTG exhaust gas flow (lb/h)- total for two CTGs (two duct burners when on)	lb/hr	6,630,800	6,973,469	7,218,232	7,578,580	5,692,996	5,888,867	6,028,774	6,258,506	5,081,836	5,240,757	5,354,272	5,539,920	6,655,108
CTG exhaust gas composition (% by volume)														
Nitrogen	%	72.64	73.47	74.37	74.82	72.93	73.82	74.63	75.07	72.93	73.77	74.56	75.04	68.31
Argon	%	0.91	0.92	0.93	0.94	0.92	0.09	0.94	0.94	0.92	0.93	0.94	0.94	0.86
Oxygen	%	12.13	12.28	12.51	12.53	13.00	13.11	13.26	13.26	12.99	12.97	13.07	13.15	9.85
Carbon dioxide	%	3.70	3.74	3.74	3.79	3.31	3.37	3.40	3.47	3.31	3.43	3.49	3.52	4.26
Water	%	10.62	9.59	8.44	7.92	9.85	8.77	7.77	7.26	9.86	8.90	7.94	7.36	16.73
NOx as NO2 (lb/h)- total for two stacks	lb/hr	44.1	46.3	48.6	51.5	34.2	35.4	36.7	38.9	30.4	32.0	33.5	34.8	55.0
based on ppmvd @ 15% O2	ppm	3.5	3.5	3.5	3.5	3.5	3.5	3.5	3.5	3.5	3.5	3.5	3.5	3.5
CO (lb/h)- total for two stacks	lb/hr	78	82	86	90	60	62	64	68	266	279	292	304	279
based on ppmvd @ 15% O2	ppm	10	10	10	10	10	10	10	10	50	50	50	50	29
VOC as CH4 (lb/h)- total for two stacks	lb/hr	9.9	10.4	10.9	11.5	14.1	14.7	15.3	16.0	12.7	13.3	14.0	14.5	24.8
based on ppmvd @ 15% O2	ppm	2.3	2.3	2.3	2.3	4.2	4.2	4.2	4.2	4.2	4.2	4.2	4.2	4.6
SO2 (lb/h)- total for two stacks	lb/hr	18.8	19.8	20.7	22.0	14.4	15.0	15.6	16.4	13.0	13.7	14.3	14.9	23.9
Particulates as PM10 (lb/h)- total for two stacks	lb/hr	38.0	40.1	42.2	44.5	32.1	33.4	34.6	36.1	28.7	29.8	30.9	32.1	45.6

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FIGURE 6 COMBINED-CYCLE GENERATION SCHEMATIC DIAGRAM



OSPREY ENERGY CENTER

DESIGN BASIS

INTRODUCTION

The Osprey Project is a highly efficient combined cycle electric power plant that will be fueled by natural gas. The Project will be nominally rated to produce 545 MW at ISO temperature and relative humidity, and 529 MW at average ambient site conditions. This Design Basis describes the Project and its supporting systems.

PROJECT LOCATION

The Osprey Project site will be located in the City of Auburndale, in Polk County, Florida, on approximately 19.5 acres situated approximately 1.5 miles southwest of downtown Auburndale and approximately 37 miles east of Tampa Bay. The site is a non-producing citrus grove zoned "Light Industry" and is currently unused. Land uses adjacent to the site include the TECO Recker Substation and 230 kV transmission line; the existing Auburndale Power Plant, which is a 150 MW natural gas-fired (with oil backup fuel) cogeneration plant owned by Auburndale Power Partners; two small residential enclaves; a cemetery; and commercial and industrial businesses. Access to the site will be from West Derby Avenue, a two-lane county collector road.

DESIGN BASIS
PAGE 2

OVERVIEW

The proposed Project will consist of two gas-fired advanced technology, dry low-NO_x combustion turbine generators ("CTGs") with the capability to use power augmentation to increase the CTGs' power output, two heat recovery steam generators (HRSGs) that include duct-firing capability to increase the steam generation capability of the HRSGs, and one steam turbine generator ("STG") rated for the full steam production capacity (including duct-firing) of the HRSGs. The CTGs will generate approximately 65 percent of the Project's output and the STG will generate approximately 35 percent of the Project's output. Thermal energy will be recovered from the hot combustion gases exiting the CTGs to generate steam in the HRSGs. Steam from the HRSGs will be expanded through an STG which will produce the remaining balance of the Project's output. This process of utilizing both the power generated in the combustion turbines as well as that generated by the STG is commonly referred to as "combined cycle" generation. To enhance power output during peak demand periods, the HRSGs are equipped with duct burners which burn additional natural gas inside the HRSGs to produce additional steam that is then used in the STG to produce additional power. Further peaking power can also be provided by extracting steam from the STG and injecting it into the CTGs. These two methods of providing peaking power will be utilized primarily during the summer months. Cooling water will be used in conjunction with cooling towers to condense steam back to water for reuse in the HRSGs. The

**DESIGN BASIS
PAGE 3**

Project's water supply will be a combination of reclaimed water and well water.

The Project will emit nitrogen oxides (NO_x), carbon monoxide (CO), non-methane hydrocarbons, small quantities of particulate matter (PM₁₀), and sulfur oxides (SO_x). The Project will be designed to control NO_x using an advanced dry low-NO_x combustion system and a selective catalytic reduction (SCR) system. This represents state-of-the-art emissions control technology, capable of achieving approximately 3.5 ppmvd NO_x levels. Only trace amounts of SO₂ will be emitted when burning natural gas. CO and non-methane hydrocarbon emissions will be minimized through the use of good combustion practice.

PROJECT DESCRIPTION

Project Structures and Buildings

The Osprey Project will include the following structures and buildings:

- A common control room, warehouse and administration building which will contain a workshop, a maintenance area, and offices.
- Each HRSG will be located adjacent to its CTG and will connect to an approximate 135 foot high emission stack. There will be one stack for each unit.
- Mechanical induced draft evaporative cooling towers.
- Water storage tanks.
- An electrical switchyard.

DESIGN BASIS
PAGE 4

Combustion Turbine Generators

The Project will employ Siemens-Westinghouse 501F industrial frame advanced technology CTGs equipped with dry low-NO_x combustors. The CTGs will be housed in an enclosure which provides thermal insulation, acoustical attenuation, and fire extinguishing media containment. The enclosure will allow access for routine inspections and maintenance.

Heat Recovery Steam Generators

One of the significant features of a combined cycle plant is the utilization of the hot exhaust gas from the CTGs to produce steam which, in turn, is expanded in a STG to drive an electric generator and produce electricity. The HRSGs are the key pieces of equipment necessary to the production of this steam. The HRSGs will be multiple-pressure, reheat units. The various pressure sections will each consist of economizer, evaporator and superheater sections. The HRSGs will also be equipped with a reheater to further improve cycle efficiency.

Steam Turbine

The STG will be a multiple admission, reheat, condensing turbine designed for sliding pressure operation. The high pressure portion of the STG receives high pressure superheated steam from the HRSG and then exhausts steam into the reheat section of the

DESIGN BASIS
PAGE 5

HRSG. Reheated steam from the HRSG is supplied to the intermediate pressure turbine, and the intermediate pressure turbine exhausts into the low pressure turbine. The low pressure turbine receives low pressure superheated steam from the HRSG and exhausts steam into the condenser.

Stacks

CTG combustion gases will discharge through two approximate 19 foot diameter, 135 foot high carbon steel stacks. The stacks will be designed to minimize the potential for aerodynamic down wash of stack emissions.

Cooling System

After the steam passes through the STG, it is condensed in a shell and tube heat exchanger (surface condenser) utilizing cooling water from the cooling tower. Each condenser will include a shell, tubes, a water box, and hot well. Condensed water in the hot well is pumped back to the HRSG to begin the thermal cycle again.

Cooling water for the condensers will be provided from evaporative (wet) induced draft cooling towers. Fans at the top of the cooling tower maintain a draft within the cooling tower. The water will be cooled by evaporation as it falls through baffles from the top of the cooling tower to a basin at the bottom of the tower where it is again pumped back through the condenser. Cooling tower components will include a basin, fans, fan decks,

DESIGN BASIS

PAGE 6

drift eliminators, fill material (baffles), and other necessary components. Average water usage will be approximately 3.55 million gallons per day when operating at full load, but without duct-firing or power augmentation, at average site conditions. Maximum water usage will be approximately 4.79 million gallons per day when operating at 95° F, 80% relative humidity while using both power augmentation and duct-firing.

Fuel Supply and Storage Systems

Natural gas will be the primary fuel for the Project. The Project's gaseous fuel system will interconnect to the Gulfstream gas metering station located on the site. The gas fuel system will also include fuel gas heaters, meters, and an isolation system in accordance with governing engineering codes.

Condensate and Feedwater Systems

The condensate system will deliver de-aerated water from the condenser hotwell to the HRSG. The condensate system will also provide water to other Project subsystems. The feedwater system will provide feedwater to the economizer sections of the HRSG. The feedwater system will also supply water to interstage desuperheaters.

Demineralized Water System

The demineralizer plant will consist of a permanently installed demineralizer system to

DESIGN BASIS
PAGE 7

produce demineralized water for the Project from the raw water source. The product water from the demineralizer system will be stored in a demineralized water storage tank for use as steam cycle makeup water.

The tank will be constructed of lined carbon steel. Demineralizer system wastewater treatment will be done on-site and then discharged to the City of Auburndale's wastewater treatment plants.

Boiler Feedwater Treatment System

The boiler feedwater treatment system would likely consist of hydrazine (or a suitable substitute) for oxygen scavenging (injected into condensate system); phosphate for boiler water solids control (utilized in the HRSG steam drums); and neutralizing amine for pH control (fed into condensate).

Wastewater Treatment System

The process waste streams will be combined, collected, and disposed of separately or in combination, depending on the type of treatment required and the ultimate discharge point. Plant wastewater that could potentially contain small quantities of oil (including wastewater from the plant area washdown floor drains, equipment and sample drains) will be treated in an oil/water separator, from which the clean effluent may be recycled for use as cooling tower makeup. Oil and sludge collected in the oil/water separator will

**DESIGN BASIS
PAGE 8**

be disposed of off-site. Wastewater grab sample points will be provided in accordance with the requirements of all applicable permits.

Sanitary waste will be discharged to the local wastewater treatment plant for disposal.

Approximately 2,880 gallons of sanitary waste will be generated per day.

HRSB blowdown will be collected in a dedicated sump and recycled to a small wastewater cooling tower before being discharged to the City of Auburndale's Allred Wastewater Treatment Plant. Cooling tower blowdown will also be routed to the Allred Wastewater Treatment Plant.

Spill prevention and control measures will include dikes around acid tanks and other chemical tanks. The dikes will be sized to contain a volume larger than that of the enclosed tank or tanks. Curbed enclosures will be provided for boiler feedwater treatment chemicals and water pretreatment chemicals.

Oil-filled transformers will be located in a sump. Storm water that collects in the sumps will drain to a common corner sump.

Compressed Air System

The compressed air system will be designed to provide dry, oil-free, control air for plant instrumentation, controls and maintenance activities.

The primary source of plant compressed air will be from permanently installed air compressors. The instrument air supply will be oil-filtered and dried. The system will

DESIGN BASIS
PAGE 9

also include a compressed air receiver.

The system will be complete with piping, valves, locally mounted instrumentation, and controls.

Fire Protection System

An on-site fire protection system will be provided for the plant. The water supply for the fire protection system will be stored on-site in either the raw water tank or cooling tower basin. A main underground fire header will be provided to serve strategically placed yard hydrants and sprinkler/deluge systems for the Project.

The fire water distribution system will incorporate sectionalizing valves so that a failure in any part of the system can be isolated while allowing the remainder of the system to function properly.

The fire protection system will also include:

- An extinguishing system for the gas turbine/generator set;
- A dry pipe, automatic sprinkler system to envelop, as required, oil piping and equipment associated with the steam turbine lubrication oil system;
- Wet pipe sprinkler systems for the turbine building and warehouse storage area;
and
- A protective signaling system with main panel in the control room.

DESIGN BASIS
PAGE 10

Control System

Each unit will have a state-of-the-art, integrated microprocessor-based control system for plant control, data acquisition, and data analysis. The plant control system will provide for startup, shutdown, and control of plant operation within limits and for protection of equipment.

Electric Power System

The electric output of each of the Project's generators will be connected to main step-up transformers. The output from the main step-up transformers will be connected to the Project's on-site switchyard.

Emissions Monitoring

A continuous emissions monitoring system for airborne pollutants will be installed to provide monitoring and alarming of NO_x and CO concentrations in the HRSG exhaust systems. The emissions monitoring system will provide input signals to the microprocessor-based data acquisition system and will meet all the requirements of the Florida Department of Environmental Protection (FDEP) for monitoring and reporting.

Stormwater Drainage

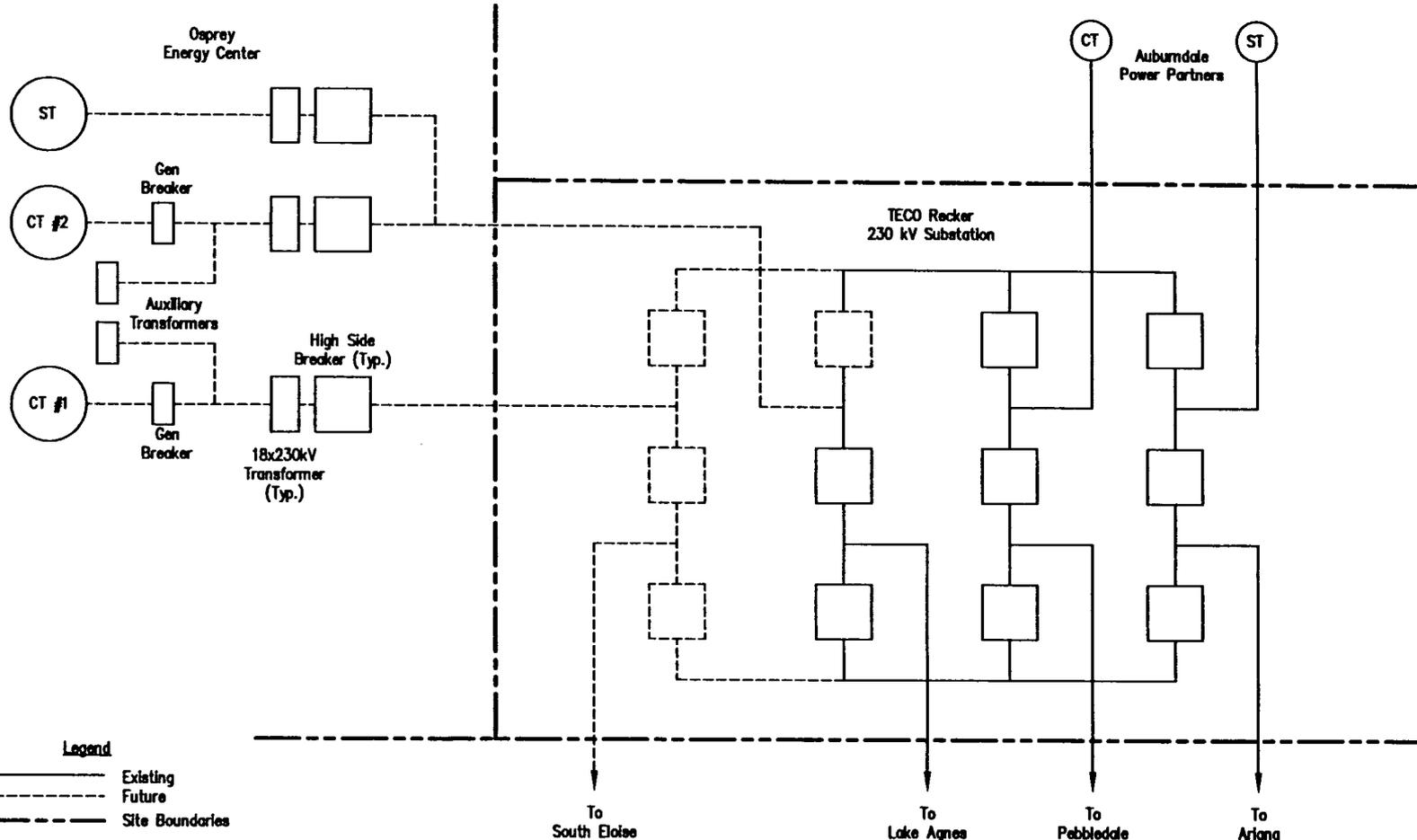
A permanent stormwater management basin will be provided to collect stormwater from

DESIGN BASIS
PAGE 11

the Project. Stormwater will be collected by a system of drains and catch basins which will connect to underground piping and swales to provide a gravity drain system. The basin will be sized to allow collected sediment to settle out before it is discharged, as well as to ensure that peak runoff rates are not increased.

Associated Facilities

No linear facilities are being permitted in connection with the proposed Osprey Project. Natural gas will be provided to the Project from a natural gas pipeline and lateral to be constructed by Gulfstream.



Legend

- Existing
- - - Future
- · - Site Boundaries

Notes:

1. Switchyard breaker ratings are 2000 amp/40 Ka typical

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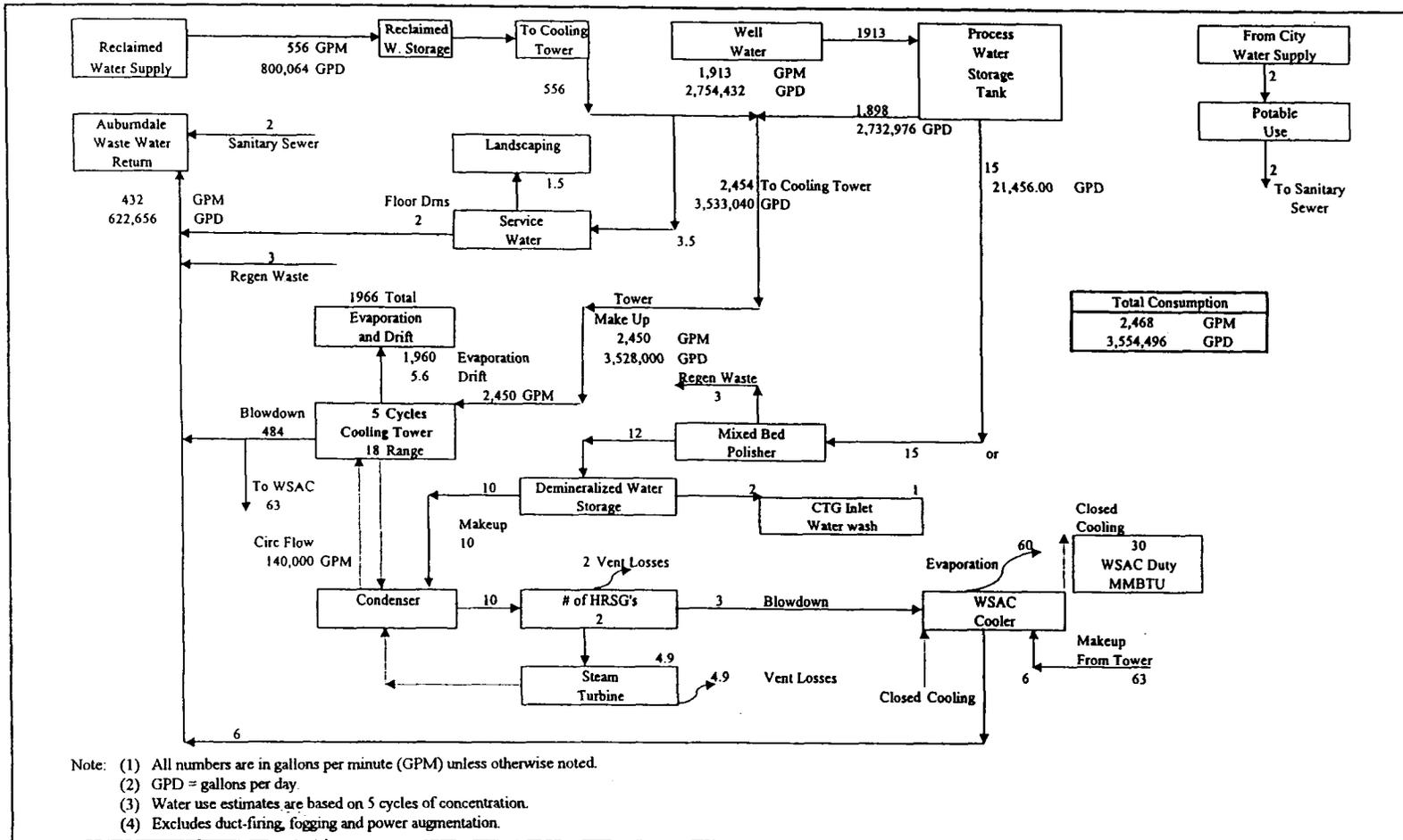
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 Osprey Energy Center

Tampa, Florida

**Station One-Line
 Electrical Diagram**

CAD BY: CDT	SCALE: NTS
CHK BY: RAZ	DATE: 08/10/00
REV BY: -	FILE No.: fig3_1_0-3.dwg

Job No. 993-9570
FIGURE Revision 01
3.1.0-3



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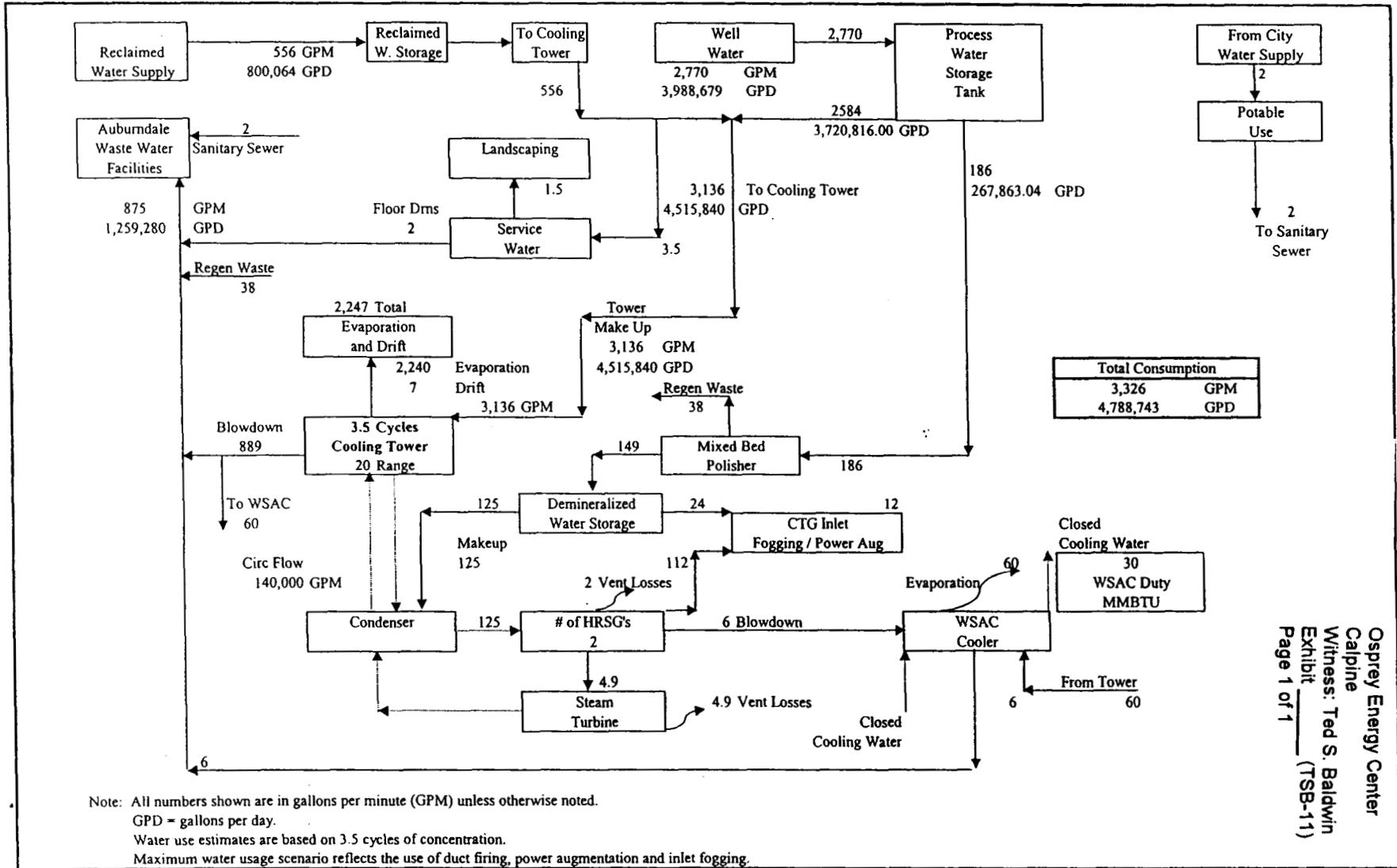
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Tampa, Florida

Average Annual Daily Water Balance Diagram

CAD BY: CDT	SCALE: NTS	Job No. 993-9570
CHK BY: RAZ	DATE: 11/29/00	
REV BY: -	FILE No.: fig3_5_0-1.dwg	



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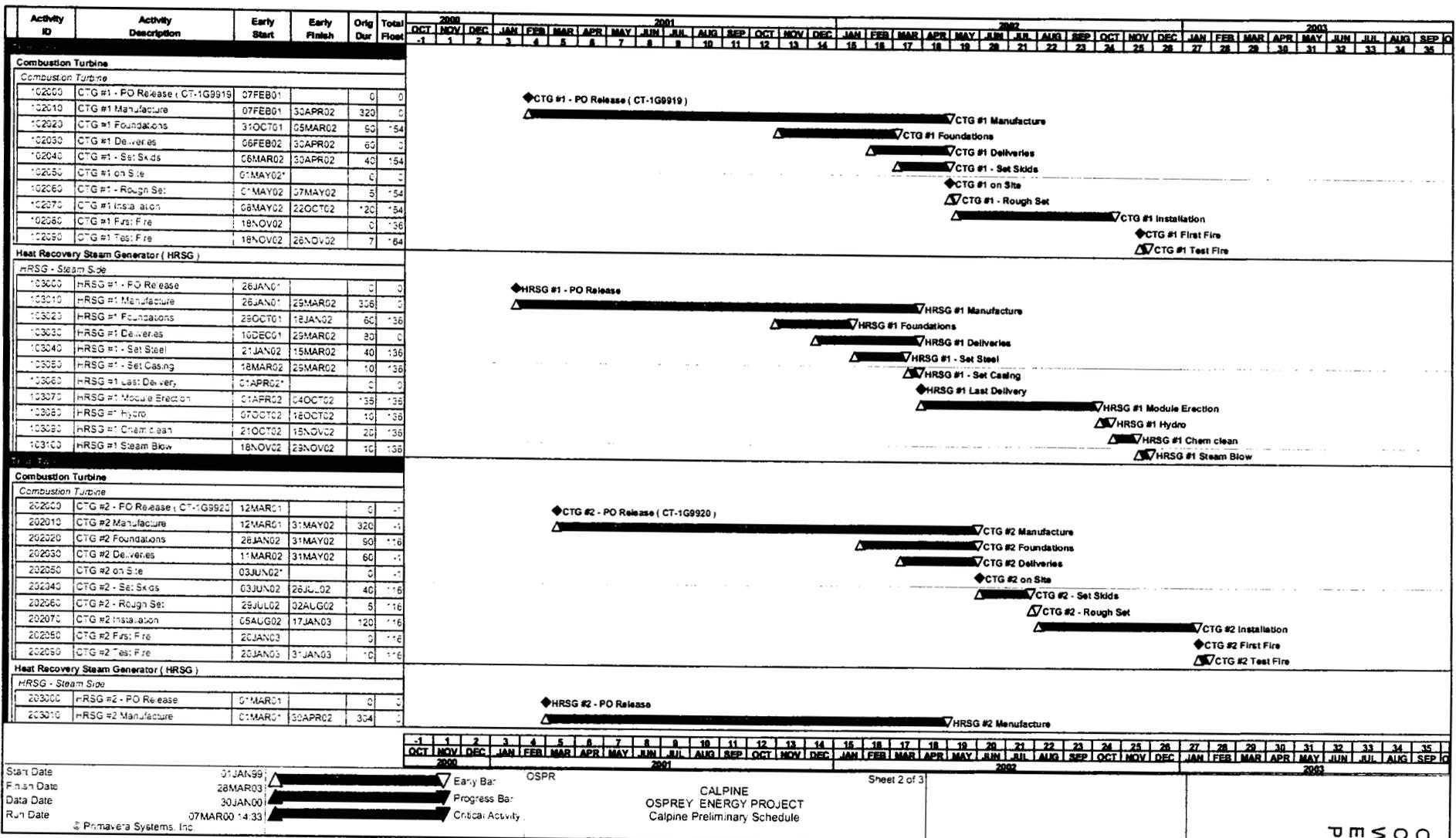
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 Osprey Energy Center

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Peak Month Daily Water Balance Diagram

CAD BY: CDT	SCALE: NTS	Job No. 993-9570
CHK BY: RAZ	DATE: 11/29/00	
REV BY: -	FILE No.: fig3_5_0-2.dwg	

OSPREY ENERGY CENTER PRELIMINARY PROJECT SCHEDULE (continued)



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 Finish Date 28MAR03
 Data Date 30JAN00
 Run Date 07MAR00 14:33

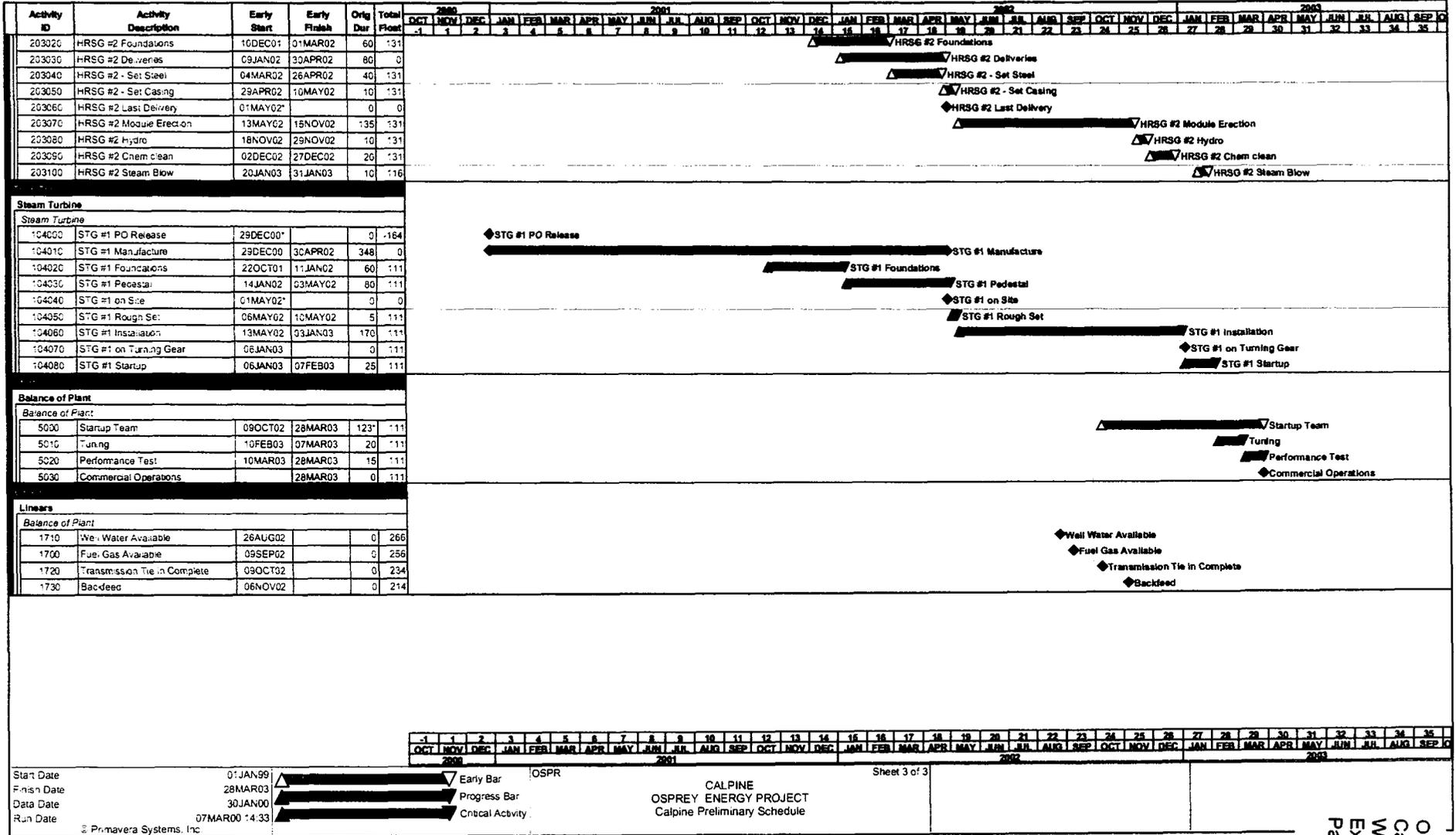
Legend:
 Early Bar
 Progress Bar
 Critical Activity

OSPR
 CALPINE
 OSPREY ENERGY PROJECT
 Calpine Preliminary Schedule

Sheet 2 of 3

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 Page 2 of 3

OSPREY ENERGY CENTER PRELIMINARY PROJECT SCHEDULE (continued)



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